

the presence of a hydrodesulfurization catalyst, thereby resulting in a liquid product stream having a sulfur content less than about 1,000 wppm;

b) passing the liquid product stream to a separation zone wherein a hydrogen-containing product gas stream and a liquid phase product stream are produced;

c) passing the liquid phase stream to a second hydrodesulfurization stage;

d) reacting said liquid phase product stream in said second hydrodesulfurization stage in the presence of a hydrogen-containing treat gas, wherein the rate of introduction of the hydrogen portion of the treat gas in this second stage is less than or equal to 3 times the chemical hydrogen consumption in this second stage, said second hydrodesulfurization stage containing one or more reaction zones operated at hydrodesulfurization conditions wherein each reaction zone contains a bed of hydrotreating catalyst, thereby resulting in a liquid product stream having less than about 100 wppm sulfur;

e) passing the liquid product stream of step d) above to a second separation zone wherein a hydrogen-containing product gas stream and a liquid phase product stream are produced.

15. The process of claim 2 wherein the Group VI metal is selected from Mo and W and the Group VIII metal is selected from Ni and Co.

16. The process of claim 1 wherein a portion of the hydrogen-containing product gas stream from the second separation zone is conducted away from the process.